

Monitoring Multiphase Flow via Earth's Field Nuclear Magnetic Resonance

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20th October 2016

Fluid Science & Resources

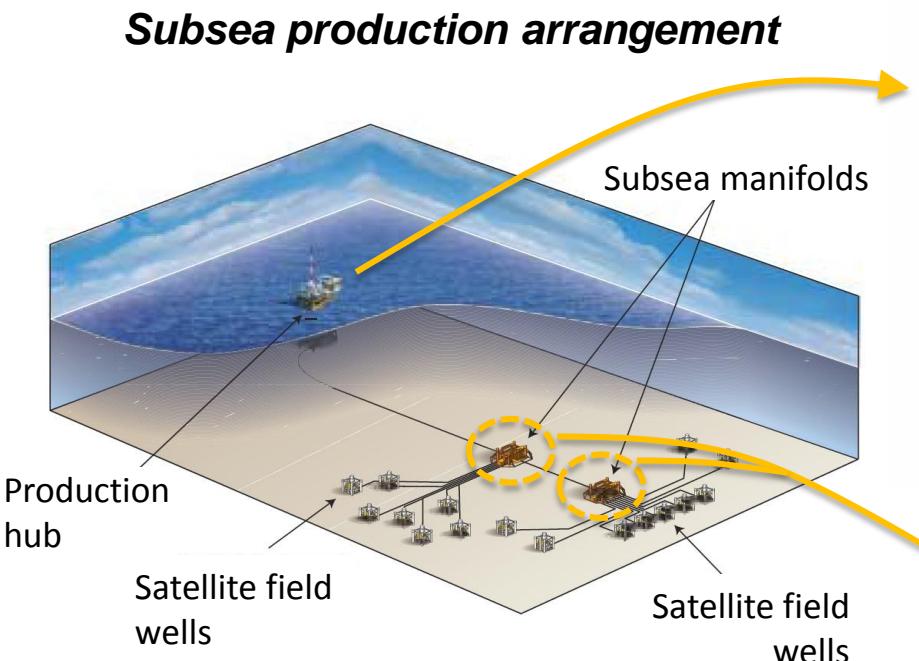
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Motivation for research



The future of oil and gas production

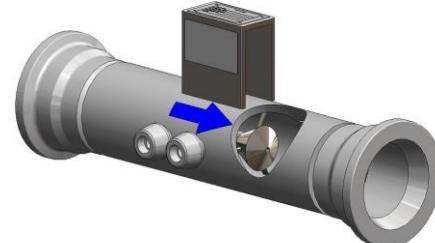
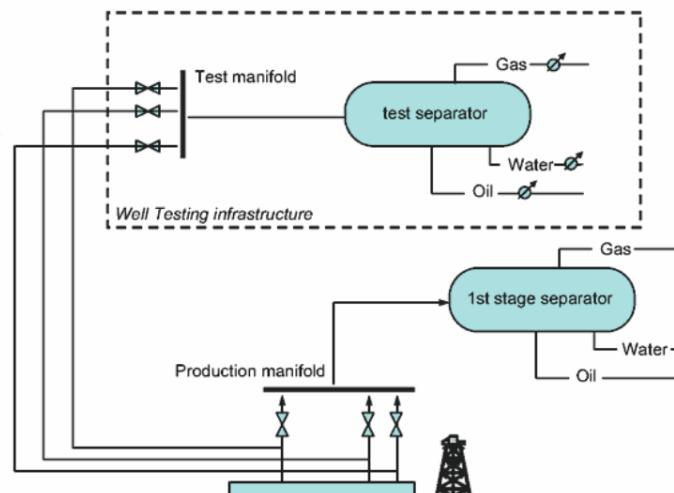
- Development of deeper offshore fields and marginal fields
- Increased produced water
- Increased subsea processing



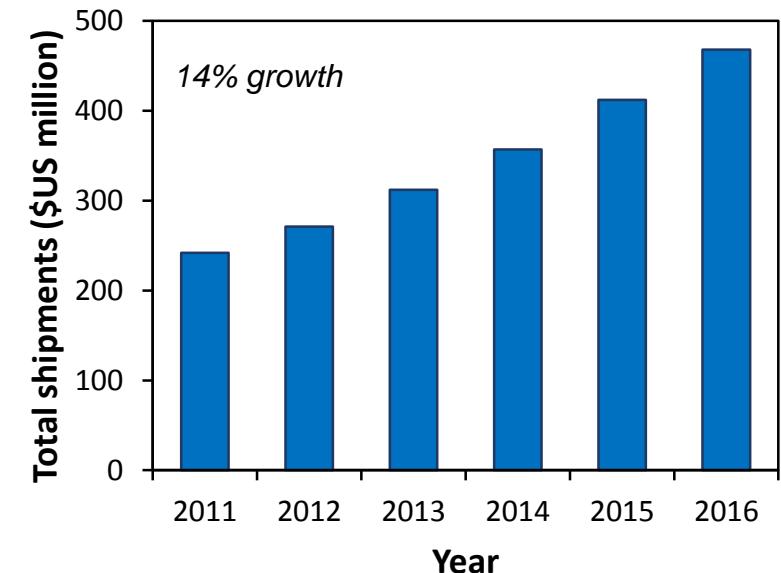
Atkinson, I., et al., A New Horizon in Multiphase Flow Measurement. Oilfield Review, 2004. 16(4): p. 52-63

Objectives of flow metering

- Measurement of phase fractions
- Measurement of phase velocities
- Flow regime identification



World Multiphase flow meter market



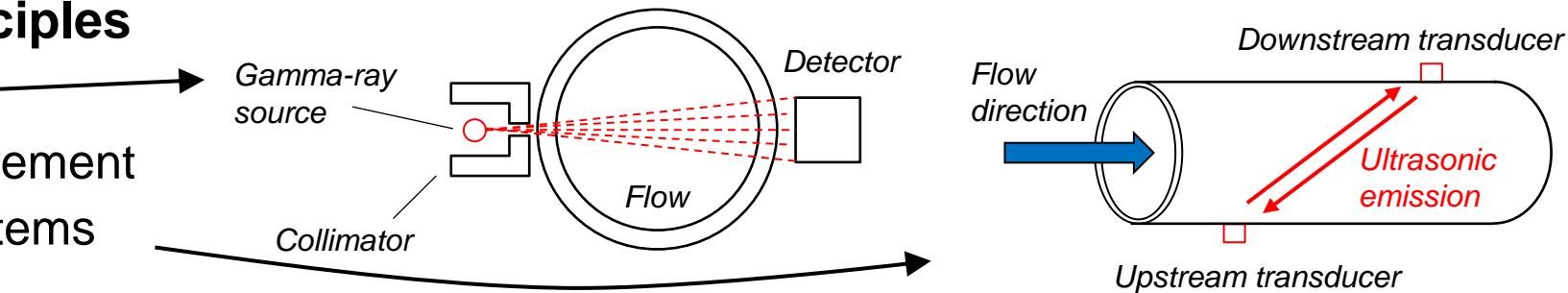
J. Yoder, *The many phases of multiphase flowmeters*, Pipeline & Gas Journal, 240 (2013) 40-41

Multiphase flow meter technologies



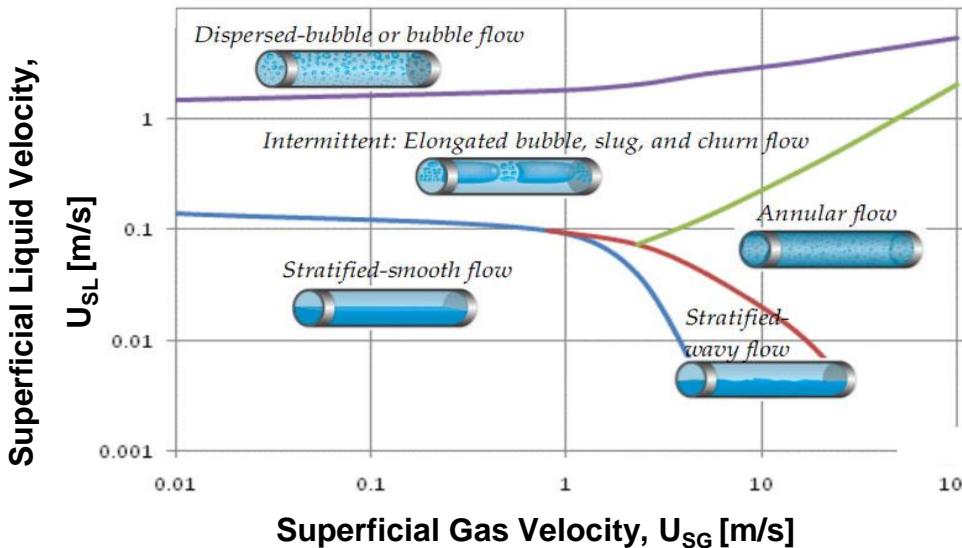
Common measurement principles

- Gamma ray attenuation
- Electrical impedance measurement
- Ultrasonic measurement systems



Advantages of nuclear magnetic resonance

- Non-invasive measurement
- Non-radioactive technology
- Flow regime independent



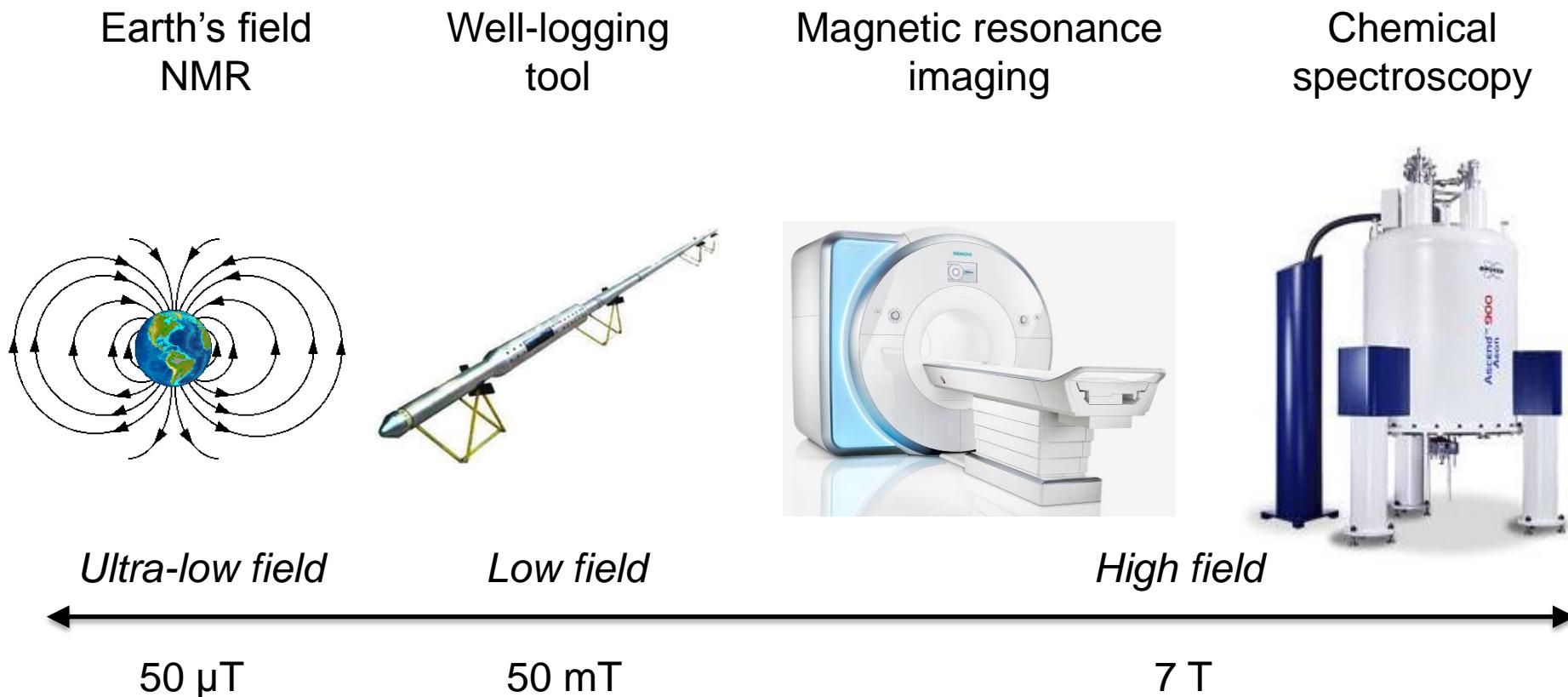
Commercial magnetic resonance flowmeter: M-Phase 5000



Nuclear magnetic resonance



Summary of nuclear magnetic resonance (NMR) magnetic field strengths

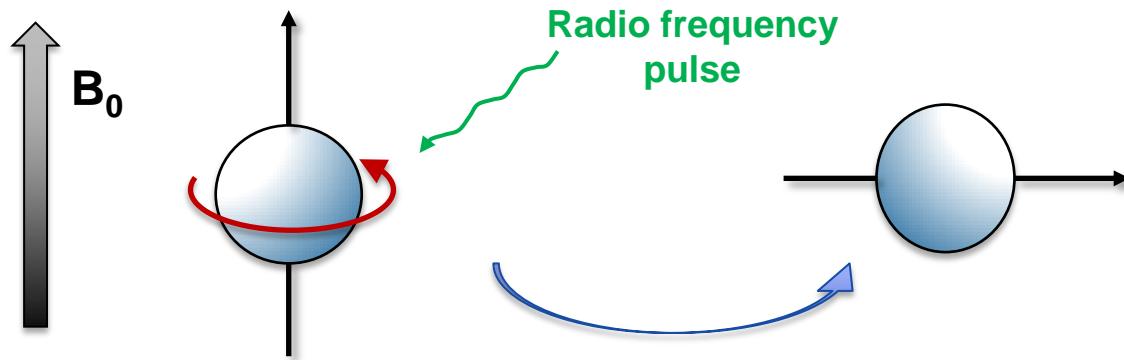


Nuclear magnetic resonance



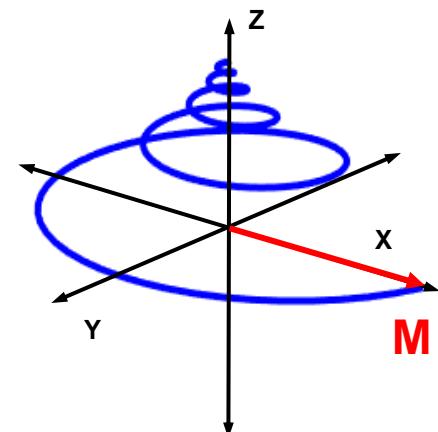
Basic classical mechanics description

1. Align nuclei (^1H atoms) with magnetic field (polarisation)

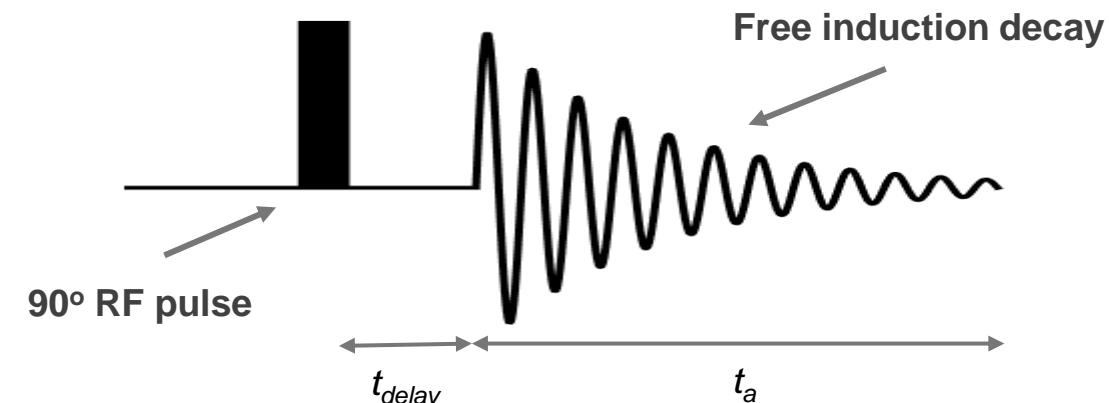


2. Apply radio frequency pulse

3. Observe the magnetisation relax



Pulse and Collect Experiment



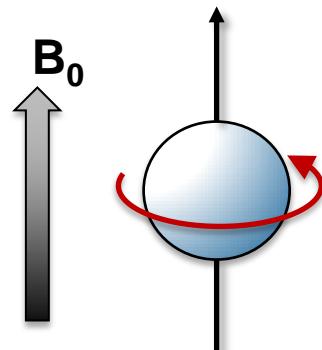
The Earth's field NMR flow meter



Key system features

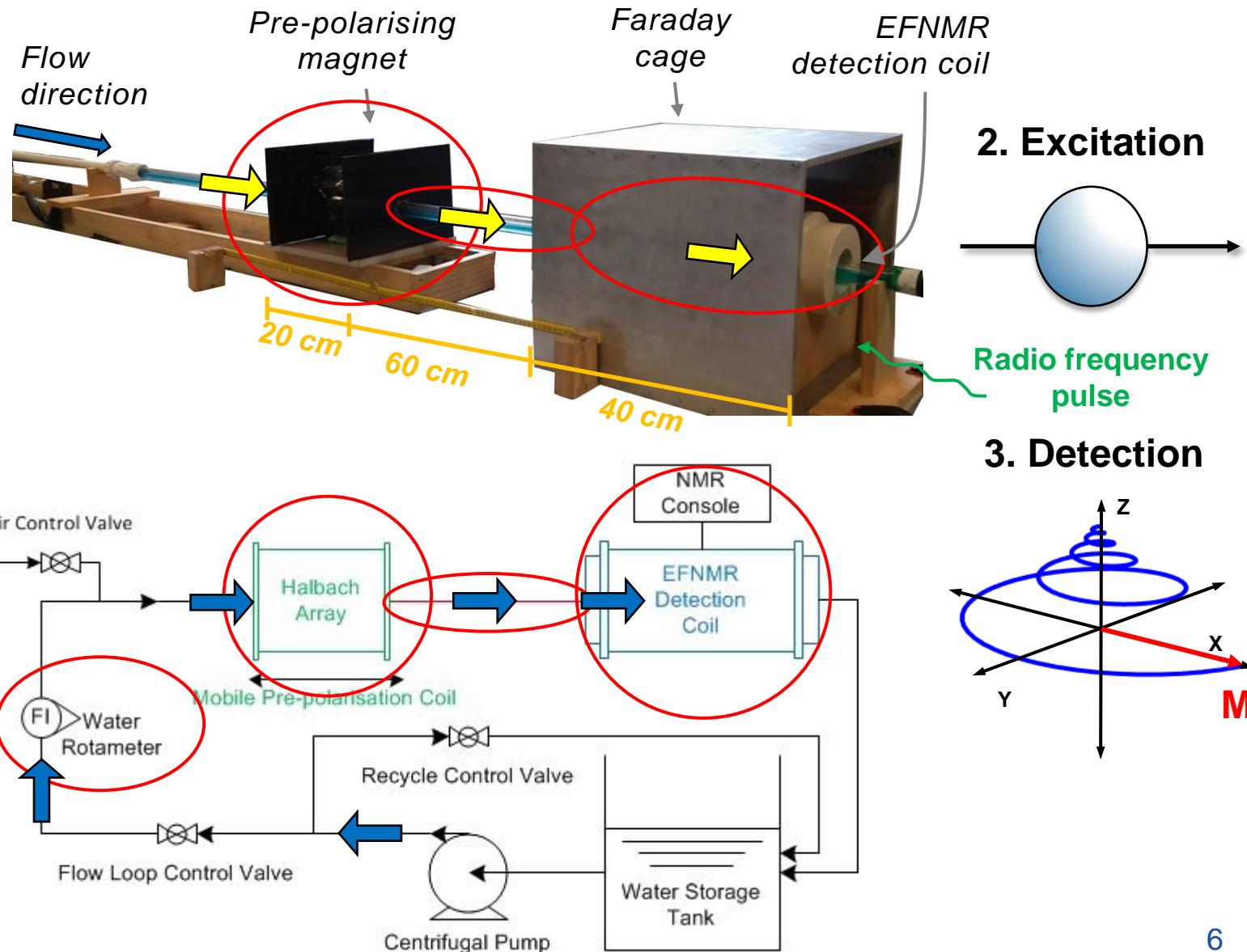
- Detected in the Earth's magnetic field
- Time of flight measurement
- Remote detection system

1. Polarisation



*Independent
flowrate
measurement*

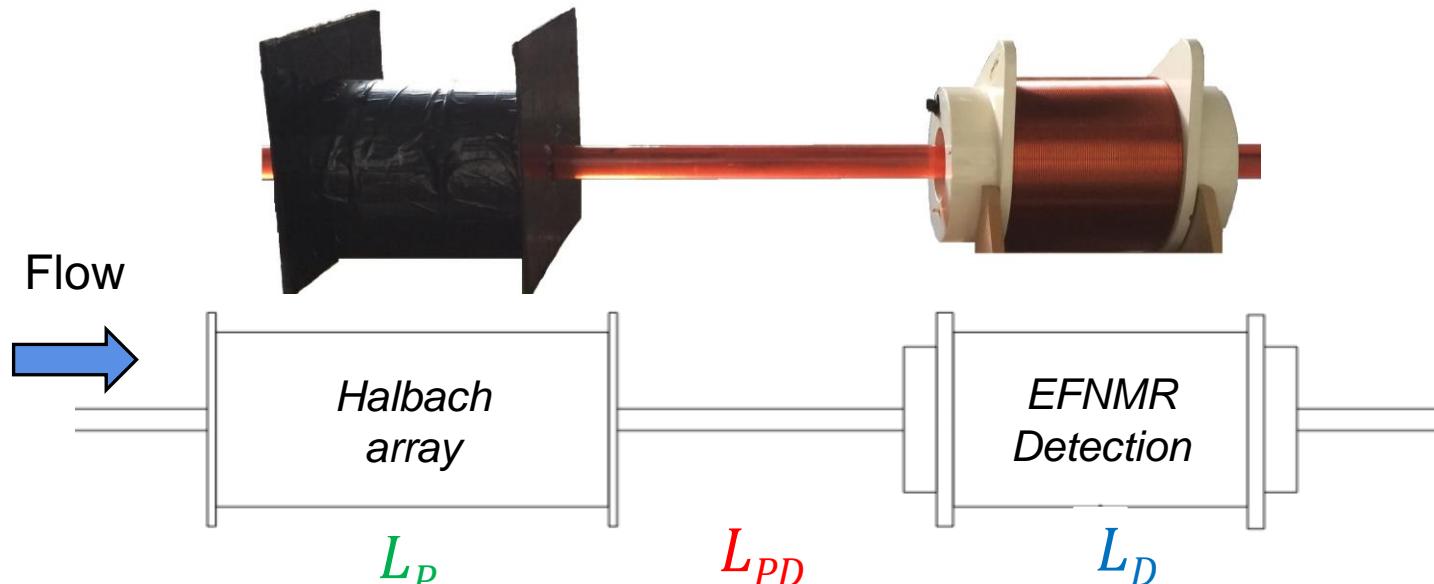
EFNMR: Earth's field nuclear magnetic resonance



Model for NMR signal



Polarisation



Flow



Halbach array

L_P

L_{PD}

L_D

$$\tau_{PD} = \frac{L_{PD}}{v}$$

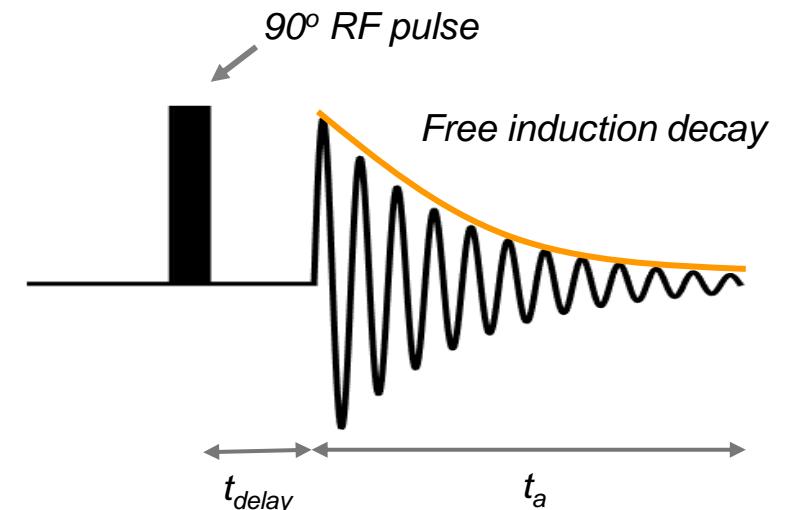
$$\tau_{PD} = \frac{L_{PD}}{v}$$

$$\tau_D = \frac{L_D}{v}$$

$$S(v, t_a) = S_0 \left(1 - e^{-\frac{\tau_P}{T_1}}\right) e^{-\frac{\tau_{PD}}{T_1}} \left(1 - \frac{t_{delay} + t_a}{\tau_D}\right) e^{-\frac{t_{delay} + t_a}{T_2^*}}$$

Detection

Pulse and Collect Sequence



Parameters

L: length

τ: residence time

v: velocity

S_0 : initial magnetization

T_1 : spin-lattice relaxation

T_2^* : observed spin-spin relaxation

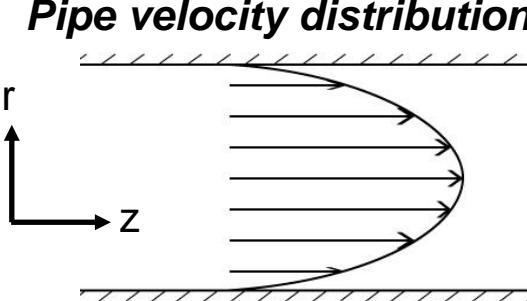
Tikhonov Regularisation



The inverse problem

$$\begin{array}{ccc} A \times P(v) = S & \xrightarrow{\hspace{1cm}} & P(v) = A^{-1} \times S \\ \text{Model transfer} & & \text{NMR Signal} \\ \text{matrix} & \uparrow & \\ \text{Velocity probability} & & \\ \text{distribution} & & \end{array}$$

Pipe velocity distribution



Real image



Image with noise



Tikhonov regularisation

- Least squares fitting method
- Allows complex models to be fit to experimental data

Reconstructed image



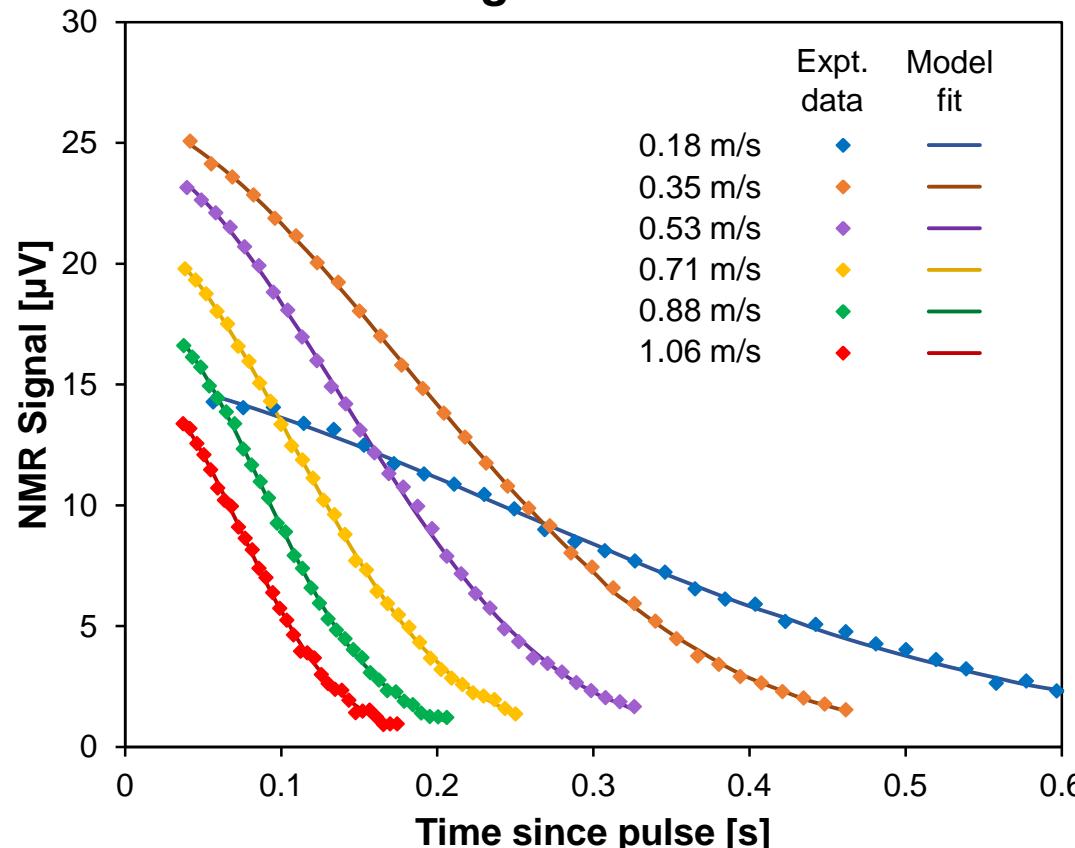
Single phase velocity analysis



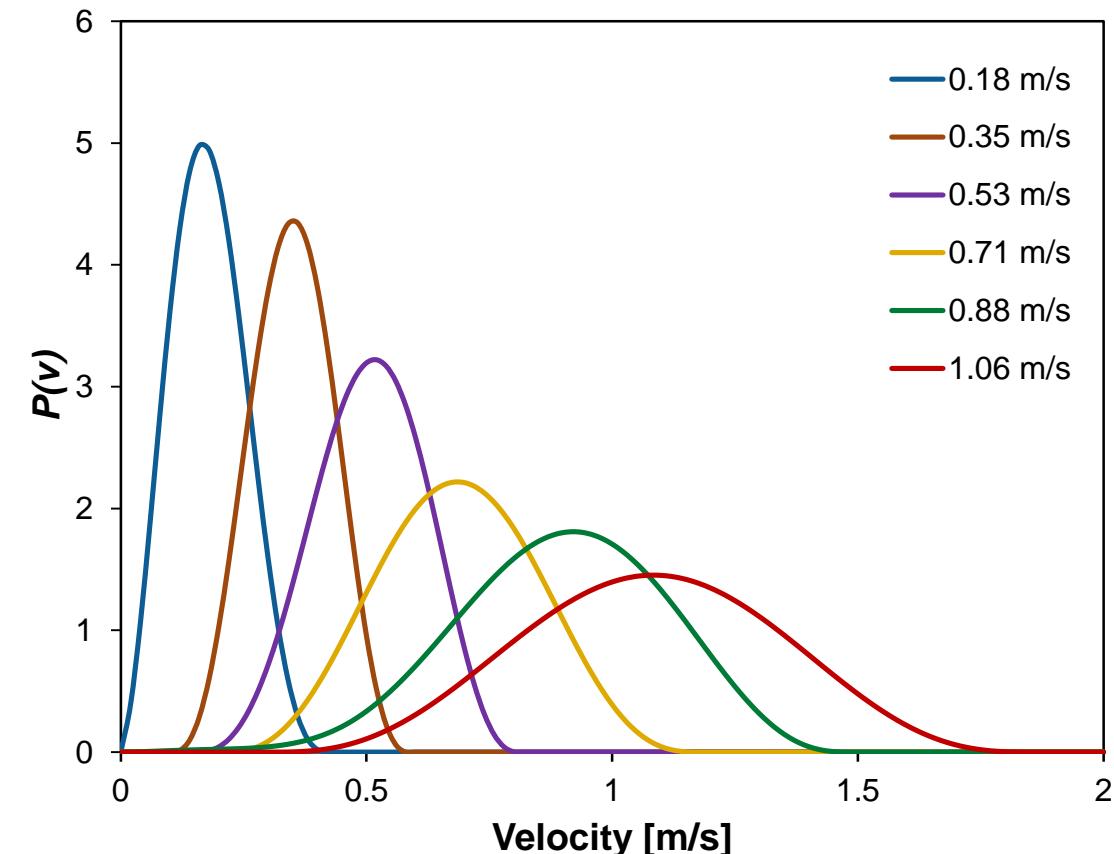
Experimental conditions

Single phase water flows at 4 – 52 L/min (0.08 – 1.15 m/s)

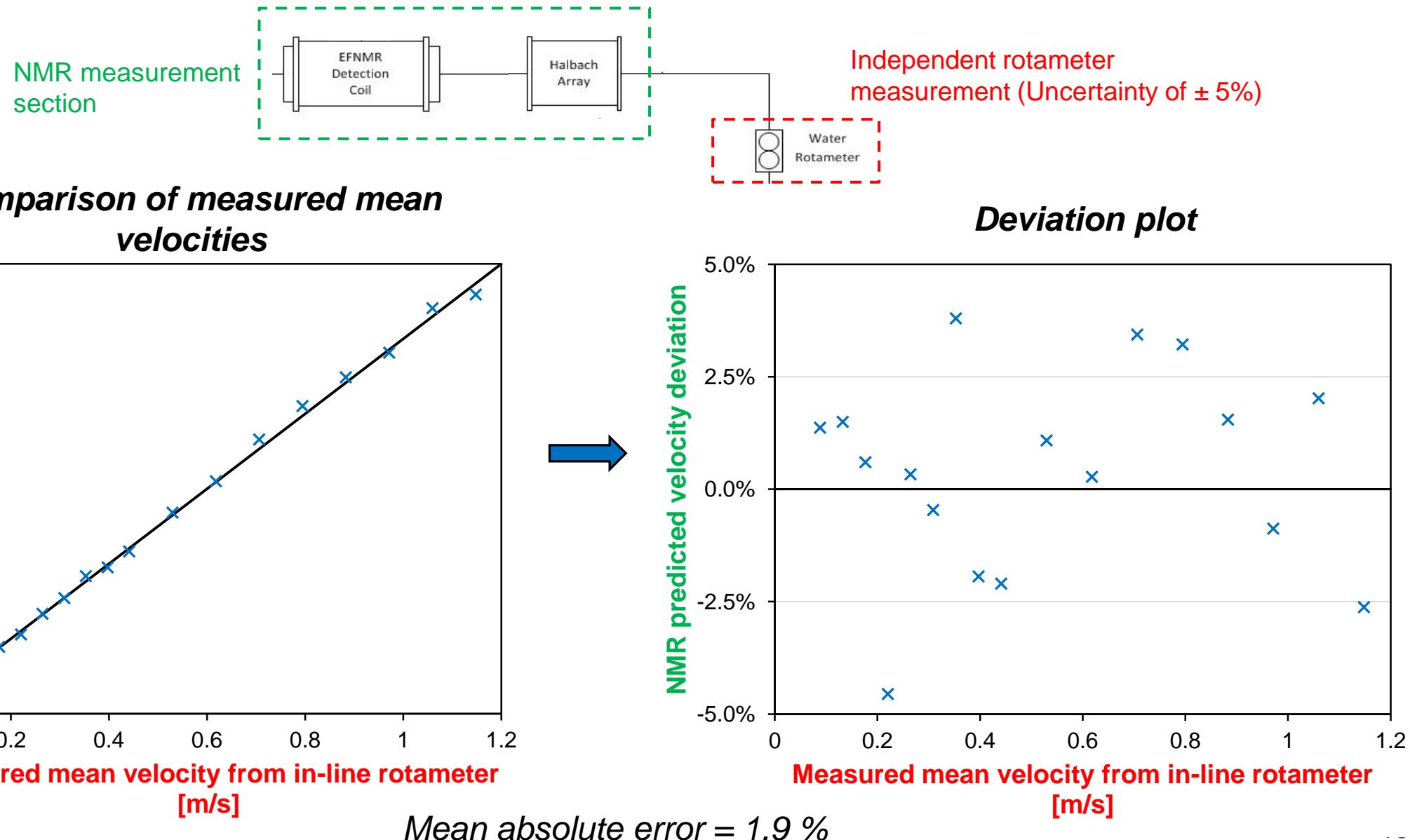
Experimental NMR signals fit using regularisation



Corresponding velocity probability distributions



Velocity comparison

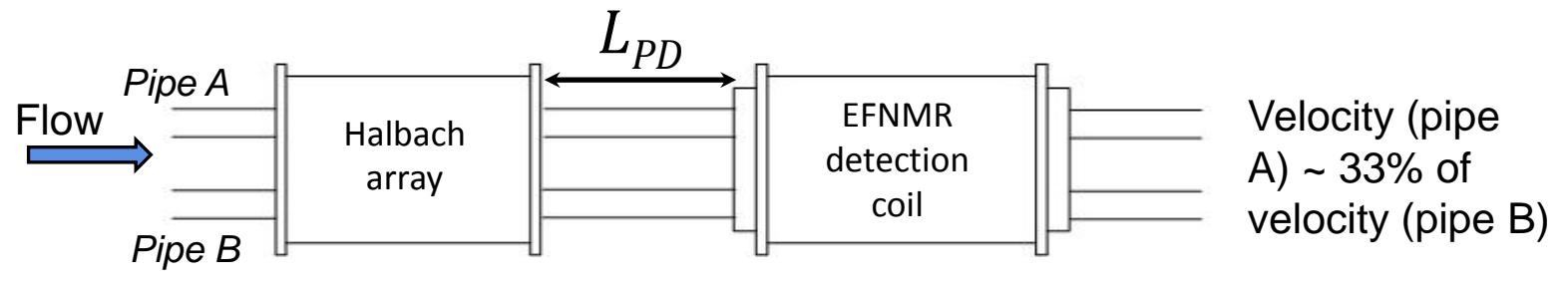


Two pipe analysis

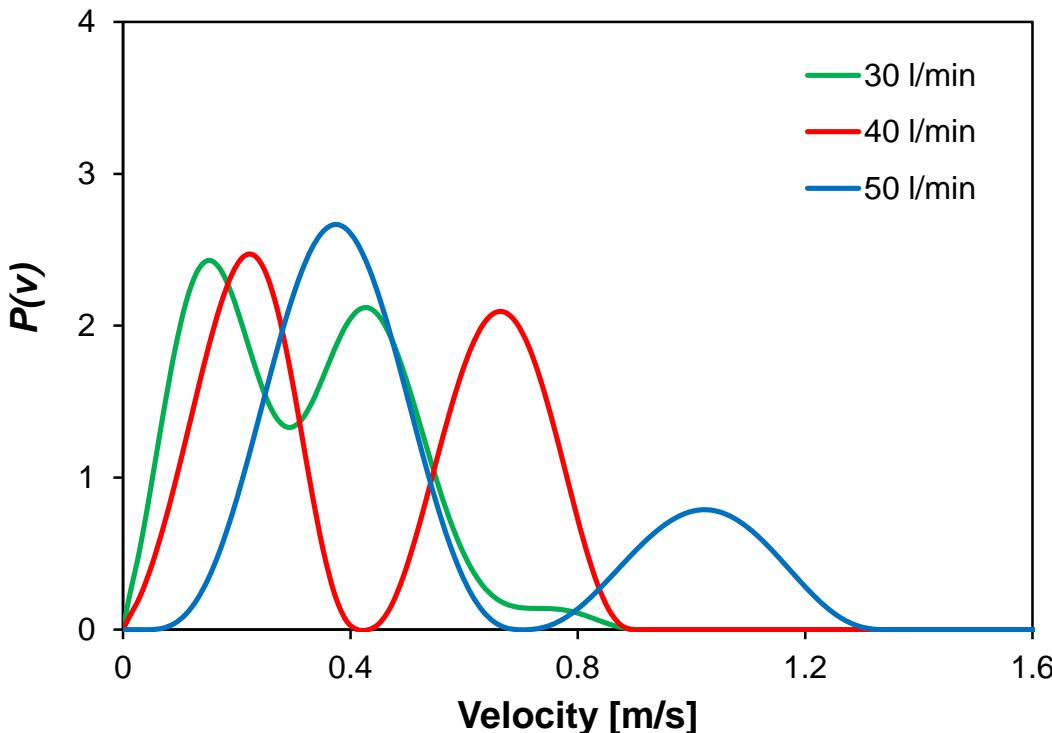


Experimental conditions

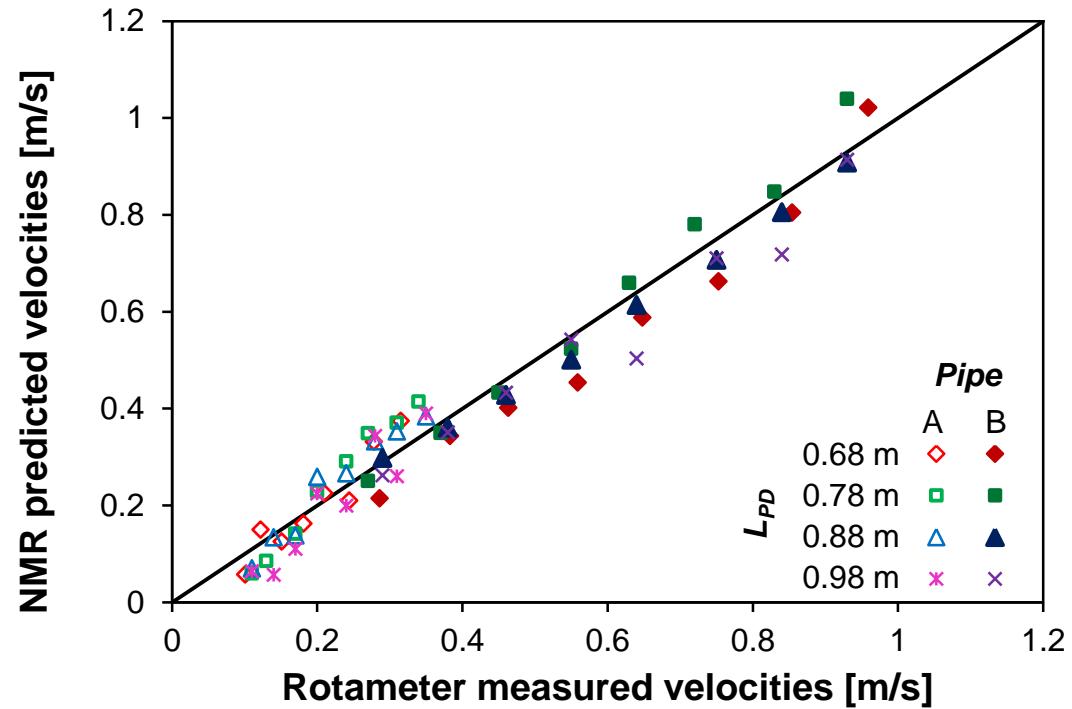
- Overall flow rates:
15 – 50 L/min
- Separation distance (L_{PD}):
0.68, 0.78, 0.88 and 0.98 m



Two pipe system velocity probability distributions



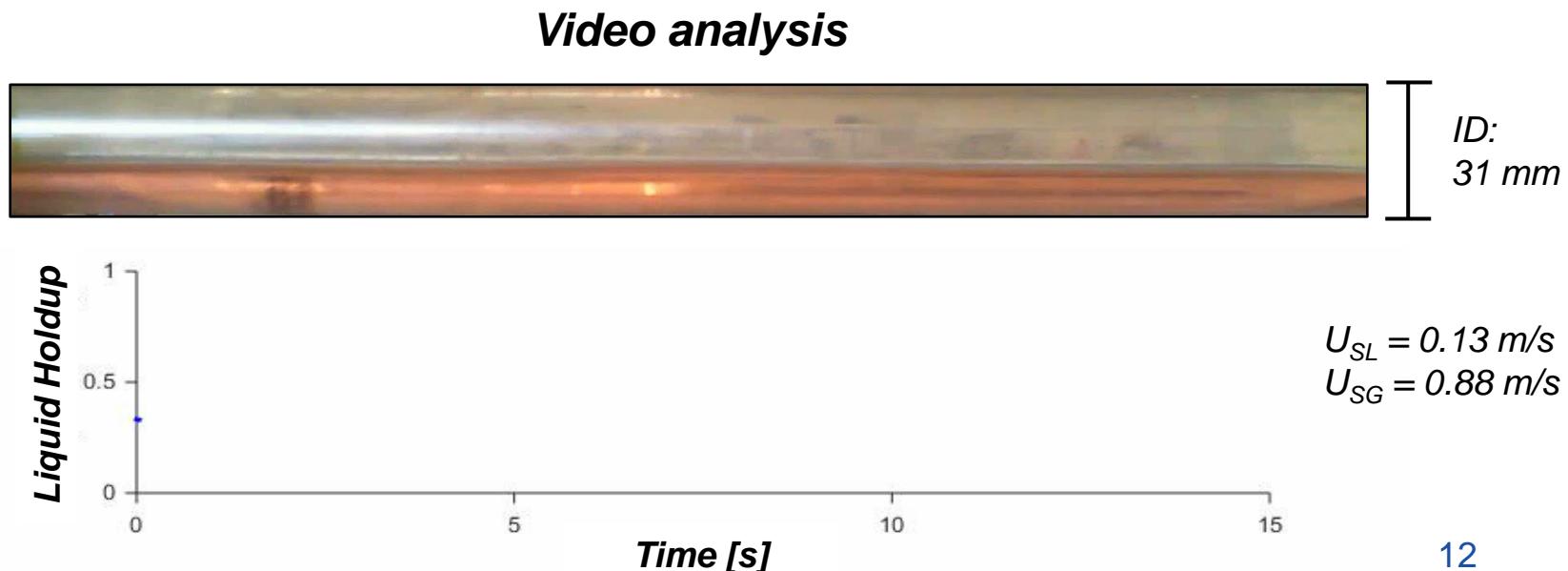
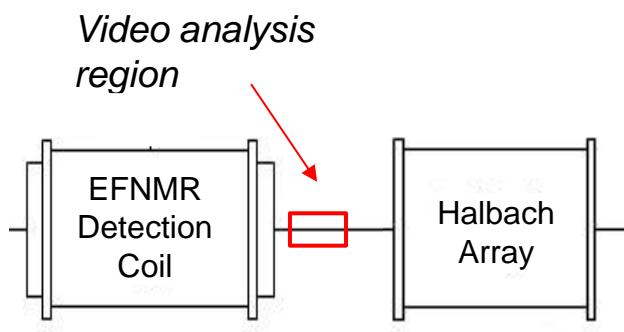
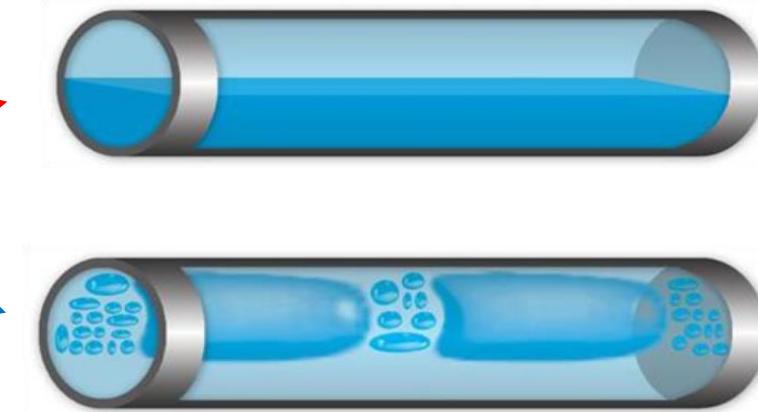
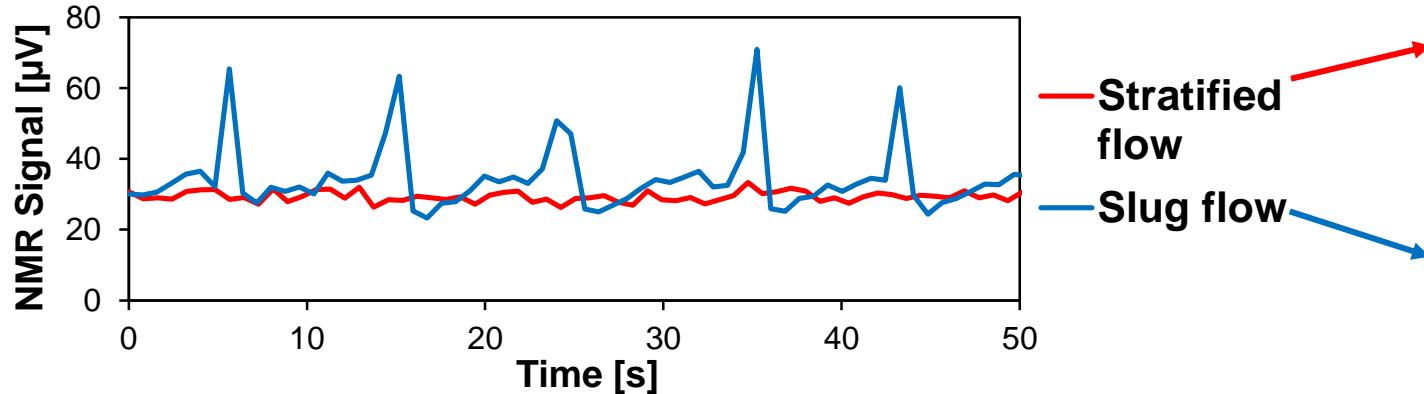
Comparison of measured mean velocities



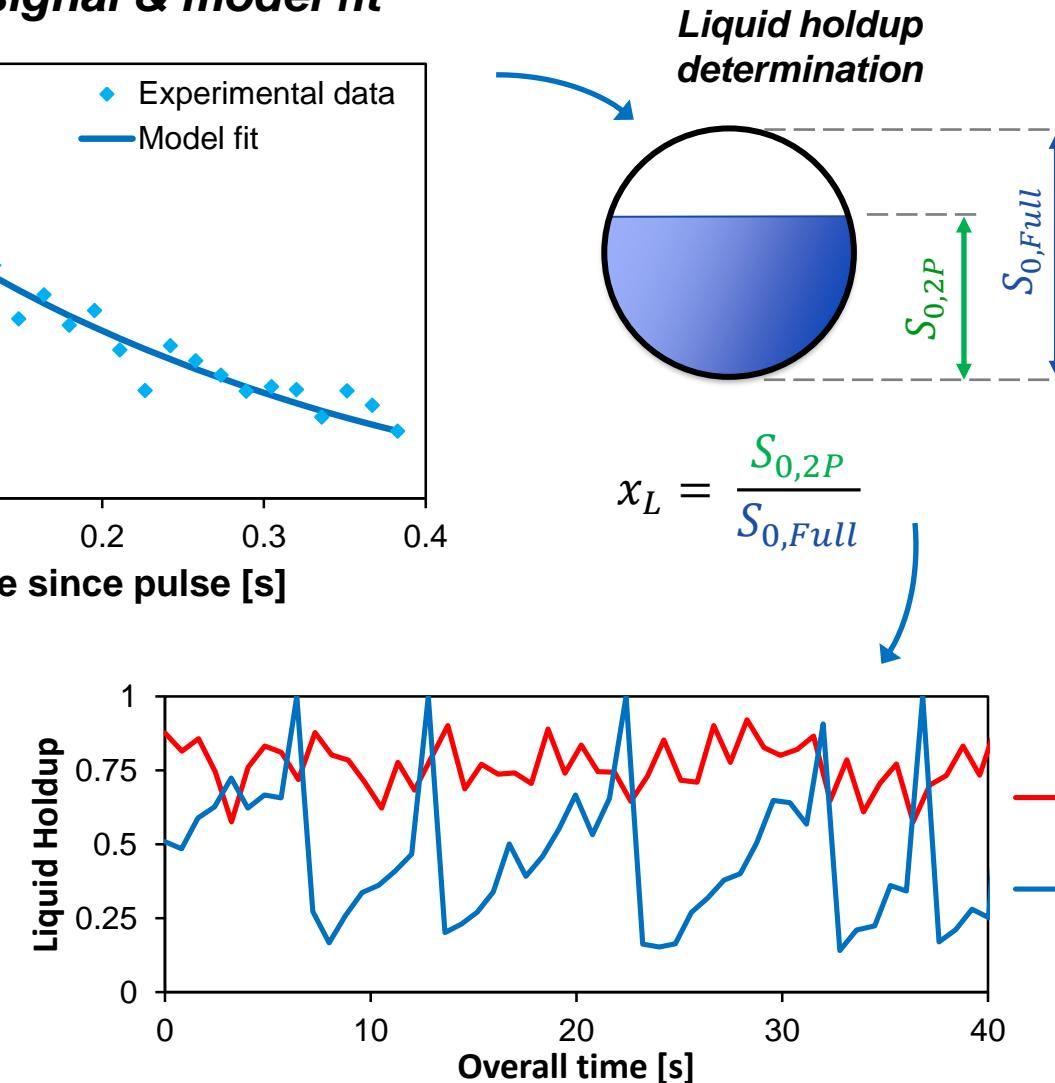
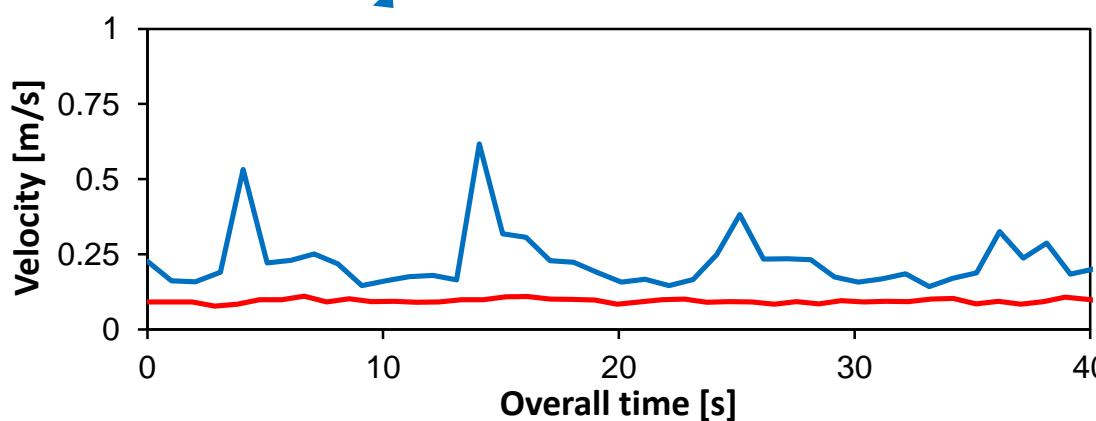
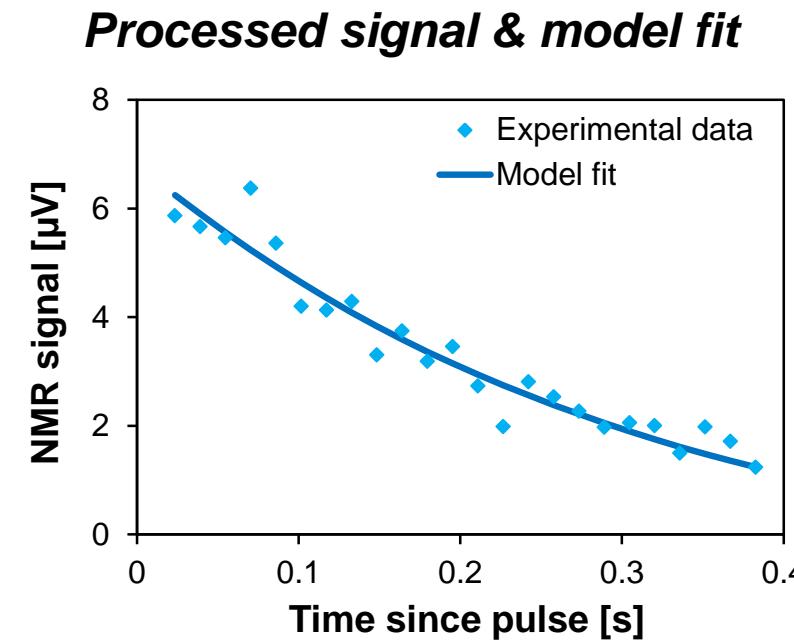
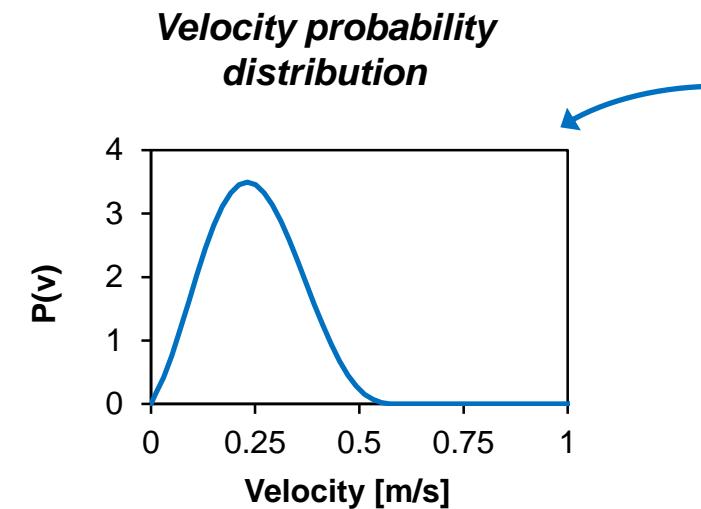
Gas/liquid analysis



Flow regime identification



Velocity and holdup determination

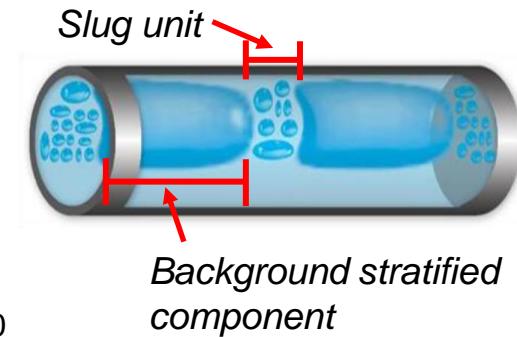
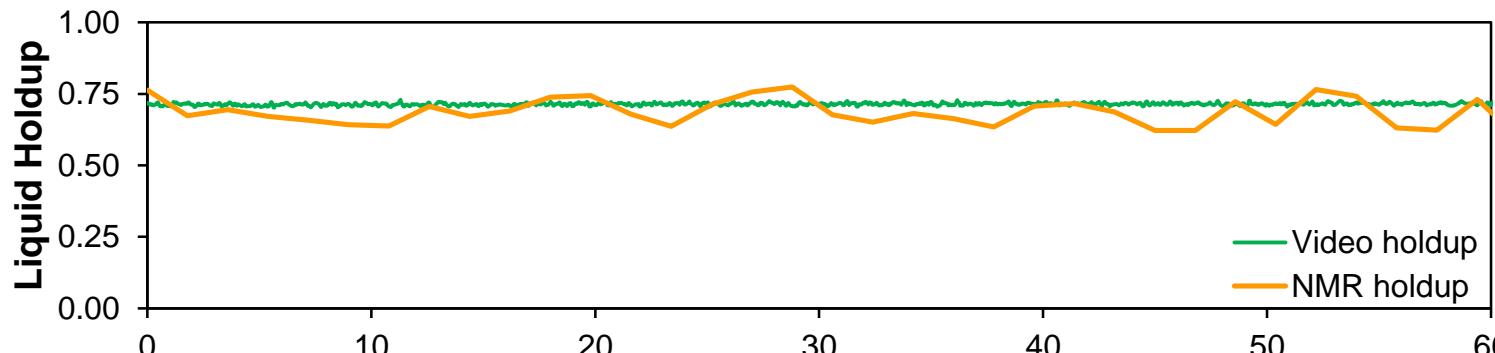


Holdup analysis comparison



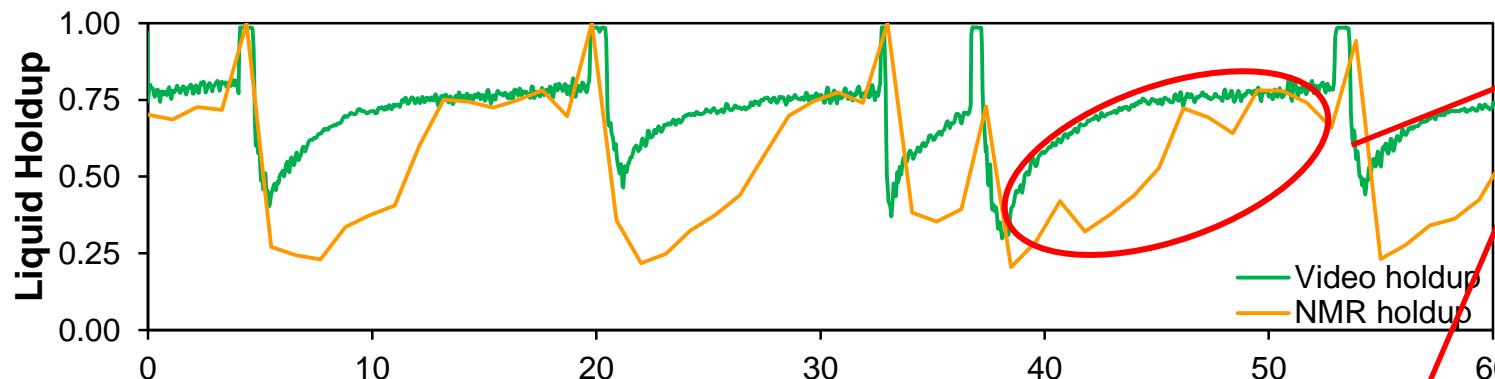
Stratified flow

Liquid: 4 L/min
Gas: 40 L/min



Low frequency slug flow

Liquid: 8 L/min
Gas: 40 L/min

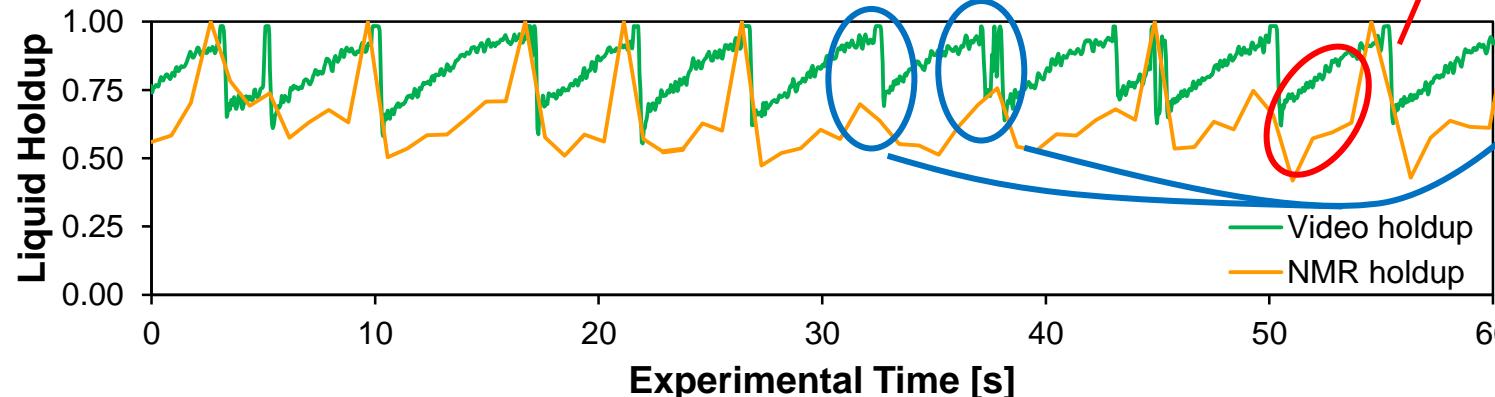


Background stratified under-prediction

- Gas bubbles
- Meniscus
- Increased relaxation

Higher frequency slug flow

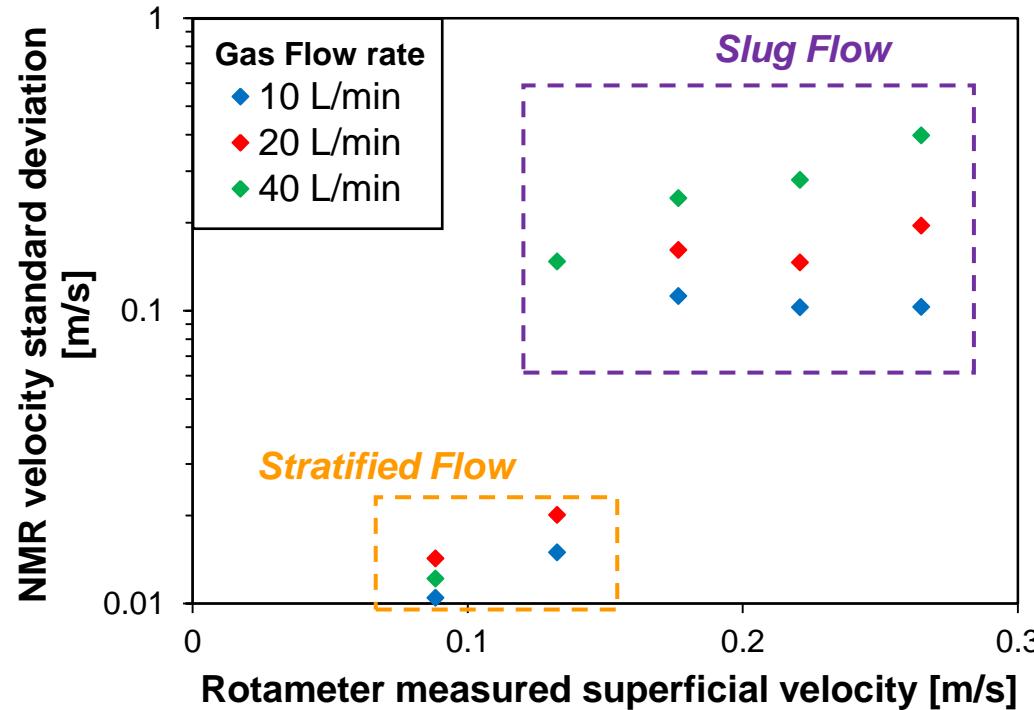
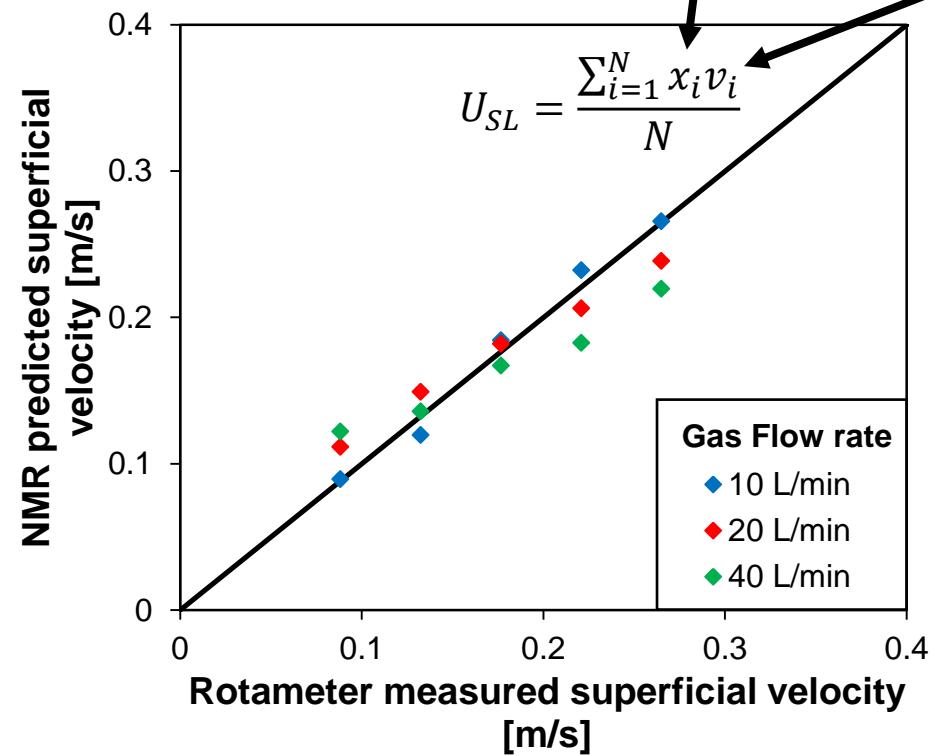
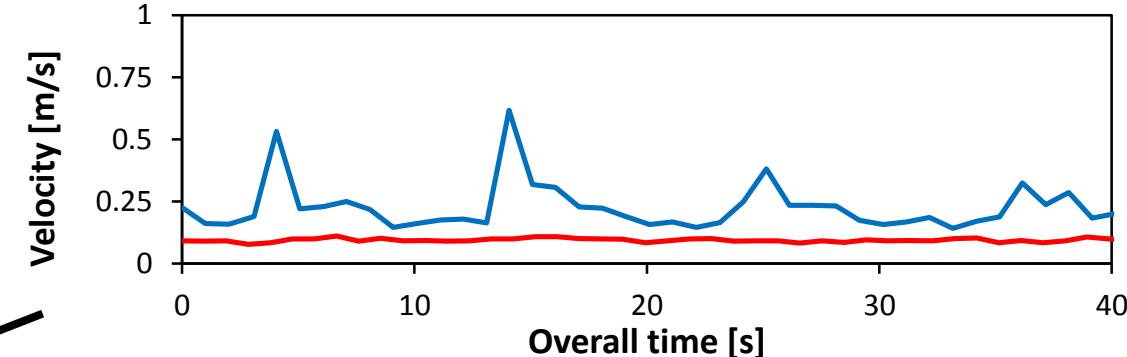
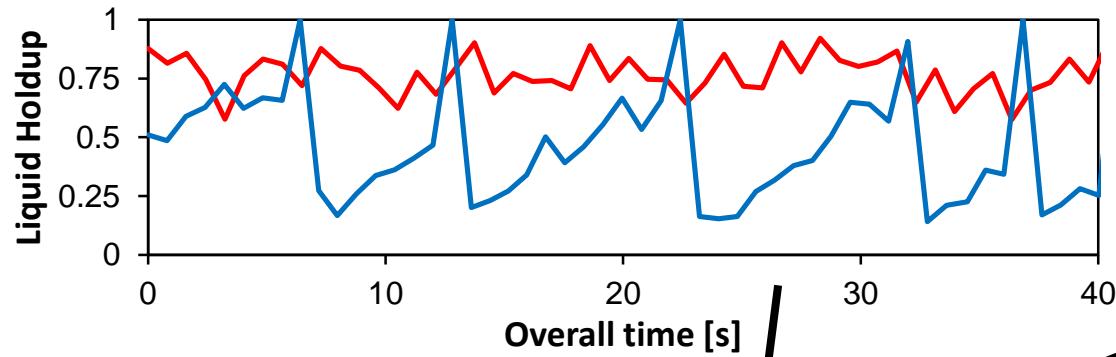
Liquid: 12 L/min
Gas: 20 L/min



Partial slug capture

- Slug residence time ~0.2 s
- Scan time ~0.7 s
- Slug not fully captured

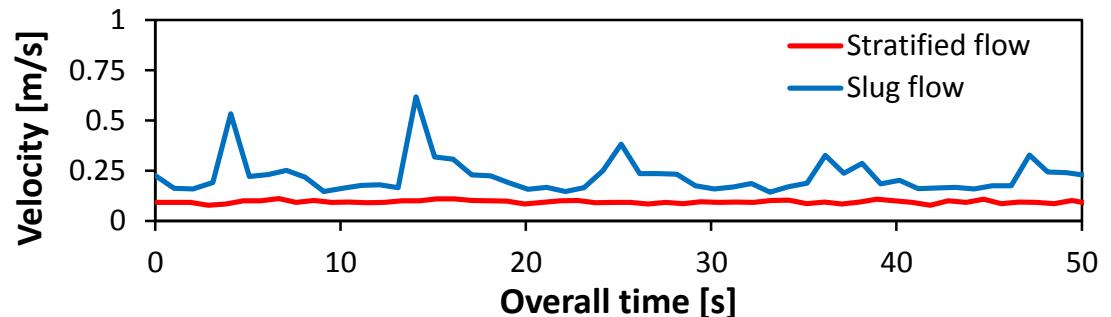
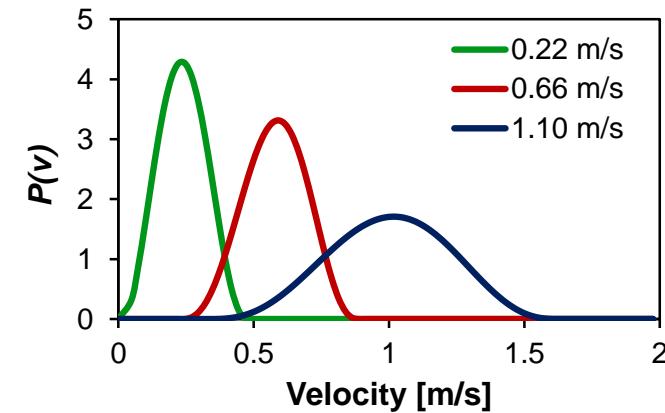
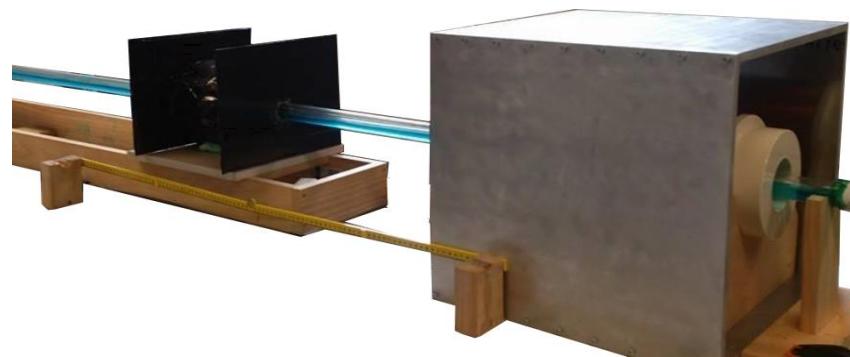
Two phase velocity analysis



Conclusions



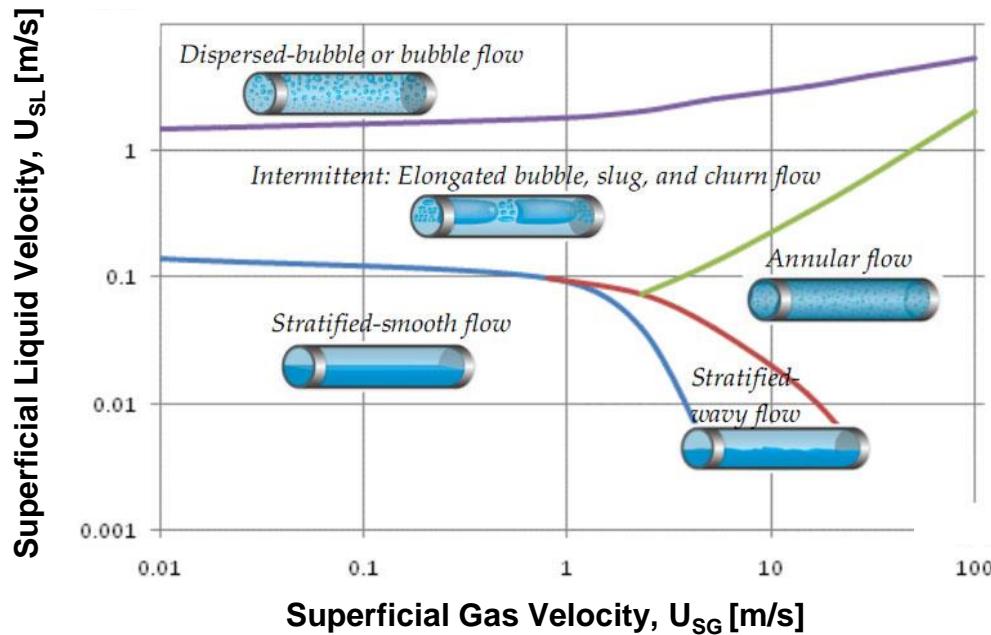
- Can accurately measure and model the FID signal of a moving fluid through the flow metering system
- Can determine the velocity probability distribution of liquid moving in the system via Tikhonov regularisation
- Able estimate the liquid velocity and holdup over time for stratified and slug flow



Future work



- Analyse fluid flow in further air/water flow regimes
- Incorporate oil into flow metering system
- Apply dynamic nuclear polarisation for signal enhancement
- Fully develop analysis techniques to be able to interpret three phase flow (oil/gas/water)



Acknowledgements



Supervisors

Michael Johns, Einar Fridjonsson and Paul Stanwix



Final Year Project Students

Adeline Klotz and Jason Collis

Thank you for your attention!

Questions?

Tikhonov regularisation



The inverse problem;

$$A \times P(v) = S \rightarrow P(v) = A^{-1} \times S$$

Model transfer matrix Velocity probability distribution NMR Signal

Apply Tikhonov regularisation;

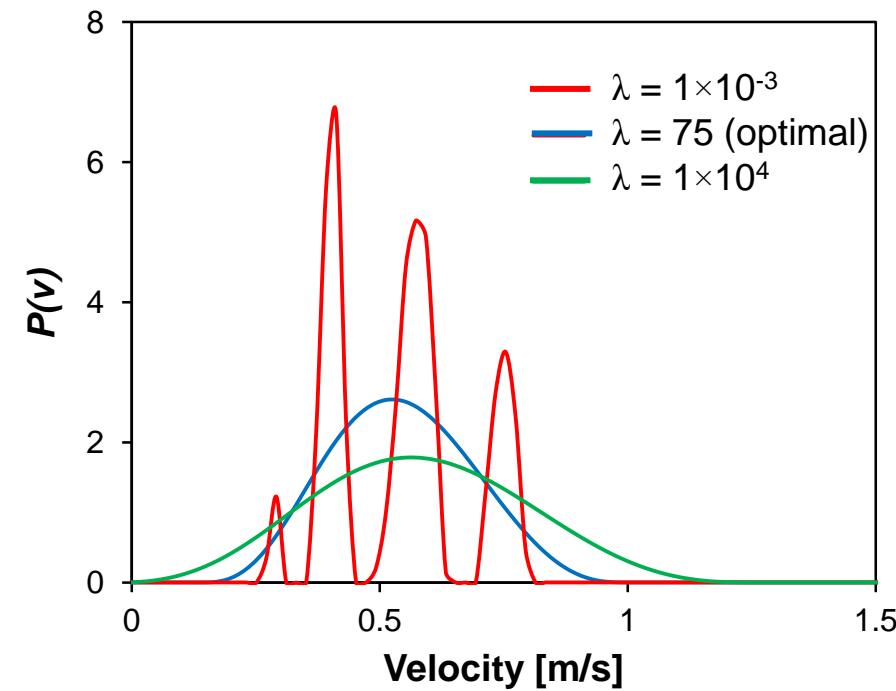
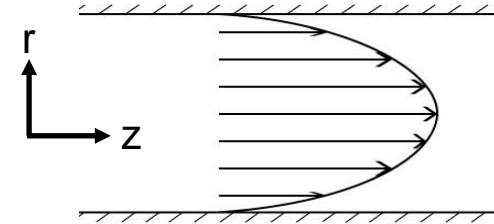
$$\min(\|A \times P(v) - S\|^2 + \lambda \|P(v)\|^2)$$

Residual norm

Second moment of $P(v)$

Generalised cross validation method is used to optimise the smoothing parameter (λ)

Pipe velocity distribution



Comparison to a theoretical model



Theoretical turbulent power law distributions

$$U(r) = V_M \frac{n+1}{n} \left(1 - \frac{r}{R}\right)^{\frac{1}{n}}$$

$$\begin{aligned} n &= f(Re) \\ n \left(0.44 \frac{m}{s}\right) &= 5.37 \\ (\text{Zagarola et al. 1997}) \end{aligned}$$

Experimental and theoretical distributions at $v = 0.44 \text{ m/s}$

